

UNITED STATES PATENT APPLICATION FOR:

**METHOD OF REMOVING CONTAMINANTS
FROM PETROLEUM DISTILLATES**

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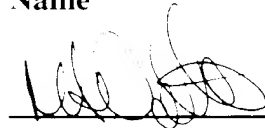
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I hereby certify that this New Application and the documents referred to as enclosed therein are being deposited with the United States Postal Service on January 2, 2001, in an envelope marked as "Express Mail United States Postal Service," Mailing Label No. EL684621983US to: Assistant Commissioner for Patents, Box **PATENT APPLICATION**, Washington, D.C. 20231.

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**METHOD OF REMOVING
CONTAMINANTS FROM PETROLEUM DISTILLATES**

5 **CROSS REFERENCE TO RELATED APPLICATION**

This application is a continuation application under 37 C.F.R. §1.53 of copending United States Patent Application Serial No. 09/465,637 filed on December 17, 1999, copending United States Patent Application Serial No. 09/250,741 filed on February 16, 1999, and copending
10 United States Patent Application Serial No. 09/265,903 filed on March 24, 1999.

TECHNICAL FIELD

This invention relates generally to the removal of contaminants from used oil, and more
15 particularly to a method of removing acidic compounds, color, and polynuclear aromatic hydrocarbons, and removing or converting heteroatoms from petroleum distillates, particularly used motor oil distillates.

BACKGROUND AND SUMMARY OF THE INVENTION

20 It has long been recognized that used motor oils can be recycled by removing the contaminants which accumulate therein during operation of the motor vehicles in which the motor oils are utilized. Recently, the American Society for Testing and Materials (ASTM) has promulgated its Designation: D 6074-99 wherein the ASTM Committee D-2 on Petroleum Products and Lubricants has promulgated standards for re-refined base oils. Included in
25 Designation: D 6074-99 are numerous attributes of base oils, including attributes relating to physical properties, compositional properties, chemical properties, and toxicological properties.

Prior to World War II used motor oil was re-refined using a process involving the addition of sulphuric acid in order to separate the contaminants from the useful hydrocarbon components of used motor oil. Re-refining processes of the type involving the addition of

sulphuric acid to used motor oil are no longer used because they result in the generation of large amounts of highly toxic acidic sludge which cannot be disposed of economically. Additionally, such re-refining techniques do not fulfill the requirements of ASTM Designation: D 6074-99.

5 More recently, used motor oils have been re-refined utilizing a process known as hydrotreating. In accordance with the hydrotreating process, used motor oils are treated with hydrogen at high temperature and pressure. Hydrotreating is successful in saturating olefins and aromatics in used motor oils and can also be used in removing heteroatoms therefrom. However, the hydrotreating process is expensive to the point that it cannot be operated profitably.

10 U.S. Patent No. 5,814,207 discloses a used motor oil re-refining method and apparatus wherein up to four evaporators are connected one to another in a series. It will therefore be understood that the apparatus of the '207 patent is expensive to install and use. More importantly, the used motor oil re-refining method of the '207 patent cannot meet the requirements of ASTM Designation: D 6074-99 because it cannot remove heteroatoms and because it cannot meet the toxicological requirements of the designation.

15 Co-pending U.S. application serial number 09/250,741 filed February 16, 1999, and assigned to the assignee hereof discloses a re-refining process wherein used motor oil is treated with an organic or inorganic base in the presence of a phase transfer catalyst. The process is successful in removing acidic compounds and color and in removing or substituting heteroatoms from used motor oil distillates. Co-pending application serial number 09/265,903 filed March
20 24, 1999, and also assigned to the assignee hereof discloses a re-refining process wherein used motor oil is contacted with a highly polar organic solvent, such as N,N-dimethylformamide. The process is successful in removing polynuclear aromatic hydrocarbons, sulphur-containing substances, nitrogen-containing substances, and other contaminants from used motor oil and distillates.

25 The present invention comprises a process for re-refining used motor oils wherein the process of application serial number 09/250,741 and the process of application serial number 09/265,903 are operated in series. The process of the invention is unique in that it is the only known process which safely and economically fulfills all of the requirements of ASTM

Designation: D 6074-99.

BRIEF DESCRIPTION OF THE DRAWINGS

5 A more complete understanding of the invention may be had by reference to the following Detailed Description when taken in conjunction with the accompanying Drawings wherein:

FIGURE 1A is the first part of a diagrammatic illustration of a method of removing contaminants from petroleum distillates comprising the preferred embodiment of the invention;

FIGURE 1B is a continuation of FIGURE 1A;

10 FIGURE 2 is the first part of a diagrammatic illustration of a method of removing contaminants from petroleum distillates comprising a variation of the preferred embodiment; and

FIGURE 2B is a continuation of FIGURE 2A.

DETAILED DESCRIPTION

15 The process of the present invention removes acidic compounds and color from used motor oil and other petroleum distillates. Additionally, the process removes and/or substitutes hydrocarbons containing heteroatoms, namely chlorine, boron, phosphorous, sulfur and nitrogen from the used motor oil. In removing these classes of compounds and to neutralize organic acids, the process uses inorganic and/or organic bases. Further, the process is capable of
20 removing polynuclear aromatic hydrocarbons from used motor oil. The process makes use of a class of catalysts known as phase transfer catalysts, which are employed in the process to facilitate the transfer of inorganic or organic bases to the substrate in the used oil.

Examples of phase transfer catalysts that may be utilized in the process include: quaternary ammonium salts, polyol ethers, glycols and crown ethers. Through either the base
25 catalysis or the neutralization reactions, undesirable components of the distillate oil are most often converted to forms that are easily removed from the used oil through distillation. Components that are not removed from the distillate are transposed to forms that may remain in the distillate with no adverse effect on the oil quality.

The invention is capable of operating in either a batch mode or a continuous flow mode. When operated in the batch mode, used oil may be contacted with a phase transfer catalyst and a base. Heat may be applied and the mixture is vigorously stirred. After the appropriate reaction time, the base and catalyst are washed out of the used oil with water, after which the remaining
5 oil is distilled. For best results in the batch process, the initial used oil should be wide cut oil prepurified by wide cut distillation.

When the process is operated in the continuous flow mode, the oil, base, and catalyst may be heated and mixed in appropriate order, passing through heat exchangers, in-line mixers, and tanks as required to effectively treat the oil. The mixture may then be passed directly to the
10 distillation apparatus, where additional mixing occurs and the catalyst and resulting oil are recovered as separate streams. The catalyst is recovered in a highly purified form and may be reused.

Although other phase transfer catalysts can be used in the process, the use of ethylene glycol is preferred because, when ethylene glycol is used, the source of the catalyst can be used
15 glycol-based engine coolants. Thus, the catalyst can be acquired in raw form with little, if any, expenditure.

Following removal of the catalyst and distillation of the lubricating oil cuts, the distilled oil is directed to a liquid/liquid extraction apparatus. The distillate and a solvent, preferably a higher polar organic solvent such as N,N-dimethylformamide, are counter-flowed through the
20 extraction apparatus, whereby the solvent removes contaminants from the distillate. Typical types of extraction devices include mixer/settler combinations, non-agitated columns, and agitated columns. The following discussion assumes the use of a Karr column, which is an agitated column design.

An exemplary process for removing contaminants from used motor oil 10 comprising a
25 continuous flow process is shown in FIGURES 1A and 1B. In the process 10, the used oil from a source 12 is passed through a used oil feed pump 14 to a heater 16. At the same time, an aqueous solution of a base, e.g., a 50% aqueous solution of sodium or potassium hydroxide, is directed from a source 18 through a base feed pump 20 and into the used oil after it passes

through and is heated to 70 to 125⁰C by the heater 16. The amount of base added to the used oil is such that the concentration of base in the oil, on a dry weight basis, is between 0.5 and 5 weight percent. The used oil and base pass through an in-line mixer 22 and a heater 24, heating the mixture to 110 to 160 ⁰C. The used oil mixture is then passed into a water flash drum 26
5 where water and a small amount of naphtha are removed through flash outlet 28. The water flash drum is best operated at low positive pressure, e.g., 0.8 to 1.1 barg., thus allowing a higher feed temperature to promote the reactions. However, in principle the flash drum could operate under vacuum. The resultant dehydrated used oil mixture is then removed from the water flash drum 26 through a flash oil outlet 30.

10 A phase transfer catalyst from a source 32 is passed through a catalyst feed pump 34 and into the dehydrated used oil mixture. The amount of phase transfer catalyst that is added to the used oil is such that the concentration of catalyst in the resulting mixture ranges from 1 to 10 weight percent of the used oil. The used oil feed pump 14, the caustic feed pump 20, and the catalyst feed pump 34 are each engaged at flow rates that provide the desired amounts of each
15 material. The used oil mixture is passed through an in-line mixer 36 and a heater 38, where it is heated to between about 275 and 350⁰C, blended with the recycled bottoms stream from recycle pump 46, passed through in-line mixer 47, heated in heater 48, and directed into a stage I evaporator 40. Heating the mixture beyond 350⁰C is not recommended as temperatures above 350⁰C can result in excessive cracking of the used oil molecules. The stage I evaporator is
20 typically operated under vacuum, with pressures ranging from about 150 to 300 millimeters of mercury. The catalyst and light hydrocarbons are removed through flash catalyst outlet 42 and the oil is removed through oil outlet 44. Part of the oil passes through a recycle pump 46 and back into the dehydrated used oil mixture after the in-line mixer 36, but before the heater 48.

The remainder of the oil passes through a stage II feed pump 49 and a heater 50, where it
25 is heated to from about 300 to 350⁰C, and into a stage II evaporator 52. The stage II evaporator operates under vacuum with pressures ranging from .5 to 5 millimeters of mercury. The stage II evaporator may be operated at lower temperatures, but this will result in a lower yield of the heavier base oil product. The stage II evaporator separates the oil into three fractions, the

viscosities of which depend upon the used oil feed. The table below lists products from a typical used oil feed:

Fraction	Color	Chlorine	Viscosity @ 40° C
light base oil	< 0.5	< 5 ppm	100 SUS
Medium base oil	< 1.0	< 5 ppm	150 SUS
heavy base oil	< 1.5	< 5 ppm	300 SUS
still bottoms	n/a	n/a	n/a

5 The light base oil is recovered through outlet 54, the medium base oil through outlet 56, the heavy base oil through outlet 58, and the still bottoms through outlet 60.

 The still bottoms resulting from the simultaneous combination of the catalyzed base treatment with distillation yields important properties when combined with asphalt. In general, the still bottoms comprise a high value asphalt modifier, capable of extending the useful
10 temperature range of most straight run asphalts. Specifically, the still bottoms impart favorable low temperature characteristics to asphalt, while maintaining the high temperature properties of the asphalt.

 Part of the still bottoms are directed through a pump 62 and are recirculated through a line 53 and the heater 50 into the stage II evaporator. The light base oil, medium base oil, and
15 heavy base oil each flow to a dedicated holding tank. Each of the base oils is fed to the extraction section in sequence in blocked operation, i.e. a tank of light base oils processed, then a tank of medium base oil, then a tank of heavy base oil, then the cycle repeats.

 Referring to FIGURE 1B, the oil is directed through a tank 68 and a pump 70 and a heat exchanger 72 to the bottom of an extraction apparatus 74, such as a Karr column.
20 Simultaneously a solvent is directed from a source 76 through a pump 78 and through a heat exchanger 80 which increases the temperature of the solvent to the top of the Karr column 74. The solvent which is utilized in the practice of the invention may be a highly polar organic solvent, such as N,N-dimethylformamide (DMF). Other solvents in the class acetonitrile may

also be used in the practice of the invention. The polarity of the solvent may be adjusted by the addition of water and/or other materials depending upon the requirements of particular applications of the invention.

5 The Karr column 74 includes a tank 82 having a rod 84 vertically disposed therein. A plurality of shelves 86 are secured to the rod 84 for vertical reciprocation thereby. The rod 84 extends to an actuator 88 which functions to reciprocate the rod 84 and the shelves 86 vertically at a predetermined rate.

10 Each of the shelves 86 has a plurality of holes formed therethrough. Because the solvent from the source 76 is relatively more dense, it tends to move downwardly in the tank 82 relative to the upwardly moving petroleum. Conversely, because the petroleum distillate is relatively less dense, it tends to move upwardly in the tank 82 relative to the solvent. The vertical reciprocation of the shelves 86 and the fact that the shelves 86 have holes therethrough substantially increases the surface area between upwardly moving petroleum and the downwardly moving solvent. By this means the solvent functions to extract contaminants which
15 are present in the petroleum distillate therefrom, and to carry the extracted contaminants upwardly out of the tank 82.

The solvent having the contaminants from the petroleum distillate dissolved therein is recovered from the tank 82 through an outlet 89 and is directed to a surge tank 90. From the surge tank 90 the solvent/contaminant solution is directed through a pump 92 and through a heat
20 exchanger 94 which increases the temperature of the solution to a falling film evaporator 96.

The falling film evaporator 96 is heated by a heating medium, e.g. steam or thermal oil, which received through an inlet 98 and recovered through an outlet 100. The falling film evaporator 96 functions to evaporate the solvent, thereby separating the solvent from the contaminants dissolved therein. The contaminants are recovered from the falling film evaporator
25 96 through an outlet 102. The contaminants flow through a surge tank 104 to a pump 106 for which directs the contaminants to suitable utilization apparatus. For example, the contaminants may be directed to an asphalt storage tank, or blended into plant fuel and burned.

The solvent is recovered from the falling film evaporator 96 through an outlet 110 and is directed to heat exchangers 112 and 118 which remove heat from the solvent. Solvent from

exchanger 118 is directed through an outlet 114 to a surge tank 116. Solvent which remains in the vapor stage is directed to a vent 122. Solvent from the surge tank 116 is directed through an outlet 124 to a pump 126 which returns the solvent to the source 76.

Petroleum distillate having the contaminants removed therefrom is recovered from the tank 82 through an outlet 130 and is directed to a surge tank 132. From the surge tank 132 the petroleum distillate is directed through a pump 134 and through a heat exchanger 136 which adds heat to the petroleum distillate to a falling film evaporator 140. The falling film evaporator 140 is actuated by steam which is received through an inlet 142 and recovered through an outlet 144.

The falling film evaporator 140 functions to remove any remaining solvent from the petroleum distillate. The solvent is recovered from the falling film evaporator 140 through an outlet 146 and is directed to heat exchangers 148 and 152, which remove heat from the solvent. Solvent recovered from the heat exchanger 152 is directed to a surge tank 150. Any solvent remaining in the vapor phase is directed to a vent 154. Liquid solvent from the surge tank 150 is directed to a pump 156 which returns the solvent to the source 76 through the tank 116 and the pump 126.

Petroleum distillate having substantially all polynuclear aromatic hydrocarbons, sulphur and nitrogen-containing substances and other contaminants removed therefrom is recovered from the falling film evaporator 140 through an outlet 160. The petroleum distillate passes through a surge tank 162 and from the surge tank 162 to a pump 164 which directs the petroleum distillate to storage facilities and/or further processing apparatus.

Referring particularly to FIGURE 1A, the water, any glycol contained in the used oil feed, and light hydrocarbons from the flashdrum 26 are directed through the outlet 28 to a condenser 170, and from the condenser 170 to a liquid/liquid separator 172. The catalyst and light hydrocarbons from the stage I evaporator are directed through the vapor outlet 42 and through a condenser 174 to a liquid/liquid separator 176. The less dense liquid from the separator 176 is directed through a pump 178 and is recovered at an outlet 180. The heavier liquid from the separator 176 is directed through pump 182 to the separator 172.

Vapors and gases from the separator 172 are vented at an outlet 184. Less dense liquid

from the separator 172 is directed through a pump 186 and are recovered at the outlet 180. More dense liquid from the separator 172 is directed through a pump 188 to a heater 190 where the heavy liquid recovers heat from the dry catalyst leaving the bottom of the distillation tower 174. Cooled dry catalyst from the heater 190 comprises dry catalyst which is returned to the source 32 through a line 192. The heated heavy liquid from the heater 190 is directed through a distillation tower 194.

The distillation tower 174 separates the feed into low boiling and high boiling cuts. The low boiling cut is directed through an outlet 196 through a condenser 198, and from the condenser 198 to a receiver 200. Gases are vented from the receiver 200 through outlet 202. Liquid from the receiver 200 is directed to a pump 204. Part of the output of the pump 204 is returned to the distillation tower 194. The remainder of the output of the pump 204 is directed to a coalescer 206. Light liquid from the coalescer 206 is directed to the separator 172 through a line 208. Waste water is recovered from the coalescer 206 through an outlet 210.

The heavy cut from the distillation tower 194 is directed to a pump 212. Part of the output of the pump 212 is directed to the heater 190. The remainder of the output from the pump 212 is directed through a heater 214 and is returned to the distillation tower 194.

FIGURES 2A and 2B illustrate an exemplary system 220 for removing polynuclear aromatic hydrocarbons and other contaminants from a petroleum distillate. The system 220 includes numerous component parts which are substantially similar in construction and function to the component parts of the system 10 illustrated in FIGURES 1A and 1B and described hereandabove in connection therewith. Such identical component parts are designated in FIGURES 2A and 2B with the same reference numerals utilized above in the description of the system 10, but are differentiated thereof by means of a prime (') designation.

The system 220 of FIGURES 2A and 2B differ from the system 10 of FIGURE 1 in that the system 220 is utilized in those instances in which the solvent is lighter, i.e., less dense, than the petroleum distillate. In such cases the solvent is directed to the bottom of the tank 82 and is recovered from the top thereof after extracting the polynuclear aromatic hydrocarbons from the petroleum distillate. Conversely, the petroleum distillate is directed to the top of the tank 82 and is recovered from the bottom thereof following removal of the polynuclear aromatic

hydrocarbons and other contaminants from the petroleum distillate by the action of the solvent. Otherwise, the operation of the system 300 of FIGURES 2A and 2B is similar to the operation of the system 10 of FIGURES 1A and 1B.

The present invention is highly successful in improving the quality of used oil distillates. Thus, in the practice of the invention, the concentration of polynuclear aromatic hydrocarbons in used oil distillates is reduced from about 200ppm to about 1ppm, or to even lower concentrations depending upon the requirements of particular applications of the invention. The use of the method of the invention is also successful in reducing the color of used oil distillates to a level comparable with that of used oil distillates that have been hydrotreated.

Although preferred embodiments of the invention have been illustrated in the accompanying Drawings and described in the foregoing Detailed Description, it will be understood that the invention is not limited to the embodiments disclosed, but is capable of numerous rearrangements, modifications, and substitutions of parts and elements without departing from the spirit of the invention.